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7 **LES AND ‘IN-VITRO’ EXPERIMENTAL VALIDATION
8 OF FLOW AROUND A TEETH-SHAPED OBSTACLE**

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21 The current paper aims to provide numerical and experimental flow data relevant for
22 physical modelling of human fricative sound production due to the interaction of air-
23 flow with the teeth. A simplified upper incisor-palate geometry is derived from typical
24 morphological features. The geometry is inserted in a rectangular channel for which the
25 width-to-height ratio yields 4. The obstruction degree due to the presence of the simplified
26 upper incisor yields 70%. Numerical flow data are obtained from large eddy simulations.
27 Experimental flow data are gathered from single-sensor anemometry on a rigid plaster
28 print of the computational grid. Transverse velocity profiles are obtained downstream
29 the constricted area, i.e. from $x = 0$ up to $x/h = 1.5$ with h denoting the aperture height.
30 The Reynolds number is set to 4000. The mean velocity profiles derived on simulated
31 and measured data exhibit a strong asymmetry due to the presence of the obstruction.
32 Nevertheless, significant differences appear with respect to the jet development, as e.g.,
33 quantified by the downstream evolution of the jet width or the appearance of signifi-
34 cant turbulence intensities ($>10\%$) at the teeth edge in the measured data whereas the
35 simulated flow remains laminar.

Keywords: Anemometry; LES; teeth-shaped obstacle; two-dimensional jet.

1. Introduction

37 Morphological teeth features, such as their exact position, orientation and shape,
38 influence human fricative sound production [Runte *et al.*, 2001]. As a consequence,
39 morphological features are of particular interest for dental prosthesis design and

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1 well documented in literature [Pound, 2001; Schierano *et al.*, 2001; McIntyre and
Millett, 2003, 2006; Rudolph *et al.*, 1998; Heydecke *et al.*, 2004].

3 In addition to available morphological characteristics, technologies such as Cone
4 Beam CT scans, e.g., used for clinical diagnoses in dental practise, are assessed
5 to obtain three-dimensional patient-specific reconstructions of oral cavity por-
6 tions. Such reconstructions are in particular useful for personalised grid reconstruc-
7 tion aiming personalised computational aero-acoustic studies [Nozaki *et al.*, 2005].
8 Nevertheless, resulting flow and acoustic data need to be validated before applying
9 such computational results for medical purposes such as dental practice.

10 In sharp contrast to morphological data, flow data issuing from configurations
11 relevant to human fricative production, i.e. moderate Reynolds Re and low Mach
12 Ma number, are few. Obviously, model validation would benefit from additional
13 flow data providing quantitative information on the mean and turbulent part of
14 the spatial velocity distribution as pointed out a.o. by Howe and McGowan [2005].
15 Recently, single sensor anemometry was applied to characterise the spatial velocity
16 distribution of moderate Re and low Ma flow issuing from an extended conical dif-
17 fuser [Van Hirtum *et al.*, 2009]. The data allowed to validate self-similar flow models,
18 which are suitable to be applied to model the airflow issuing from a constriction
19 between the tongue and the palatal plane. Although, no obstacle was considered
20 and no computational results were provided.

21 ‘In-vitro’ mechanical models of simplified geometries suitable to study fricative
22 sound production are few. A rectangular obstacle downstream an obstruction was
23 considered by Shadle [1985] in order to study the influence on the sound produced,
24 so no detailed velocity flow data were gathered.

25 The present research aims to provide velocity data downstream an incisor-shaped
26 obstacle in a rectangular uniform vocal tract for an airflow with moderate Re -
27 number set to $Re = 4000$. The chosen Reynolds number is well within the range
28 typical for fricative sound production $2000 < Re < 10^4$ [Stevens, 1998; Howe and
29 McGowan, 2005]. The obstruction degree yields 70% and the width-to-height ratio is
30 set to 4 to ensure two-dimensional flow. A comparison of experimental and numerical
31 mean and turbulent velocity data is provided in the near flow field downstream the
32 obstacle from $x = 0$ up to $x/h = 1.5$ where h denotes the aperture. Both the inner
33 and outer layers of the jet issuing from the aperture are sought. The characterisation
34 is inspired on features commonly observed for plane wall jets since a two-layer shear
35 flow can be expected [Launder and Rodi, 1983; Eriksson *et al.*, 1998; Townsend,
1999].

37 **2. Geometry of Interest: Palate-Teeth Shaped Obstacle and Nozzle**

38 Dental dimensions and measures are reported in literature with increasing precision.
39 High precision is required for sophisticated dental surgical techniques and the devel-
40 opment of personalized denture services such as dental prosthesis. In this section, a
41 simplified two-dimensional teeth-shaped obstacle geometry is derived from reported

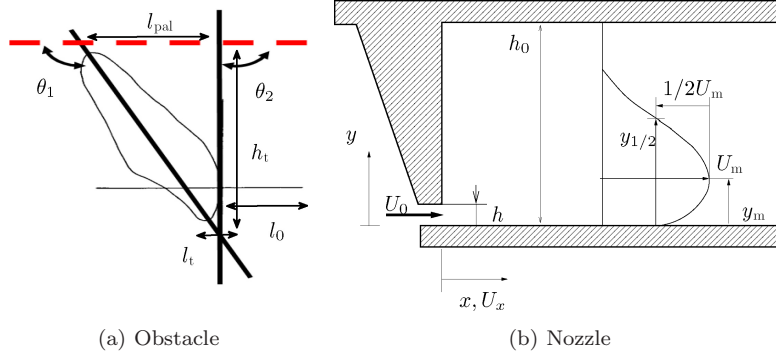


Fig. 1. Schematic illustration of (a) two-dimensional teeth-shaped obstacle (bold lines) in relation to upper incisor morphological data [Fredericks, 1974; Ellis and McNamara, 1986]: the palatal plane is indicated as a dashed line and (b) resulting teeth-shaped nozzle and some major geometrical and flow parameters derived from plane wall jet nomenclature [Eriksson *et al.*, 1998]: transverse flow direction y , longitudinal flow component $U_x(x)$ in the main flow direction x indicated by a bold arrow, characteristic velocity at the constriction outlet U_0 at $x \approx 0$, aperture height h , channel height h_0 , $y_m(x)$ distance from the wall up to the position of maximum flow velocity $U_m(x)$ in the transversal velocity profile, $y_{1/2}(x)$ distance from the wall up to the outer position where the velocity corresponds to $U_m/2(x)$.

1 upper teeth incisor measures. In the simplified geometry, schematically illustrated
 2 in Fig. 1, the palatal plane is represented by a flat plane and the upper teeth geome-
 3 try is represented as a trapezoid connected to the palatal plane, i.e. the upper teeth
 4 consists of four straight plates. This way, in particular two morphological features
 5 are accounted for in the current upper teeth-shaped obstacle:

- 6 (1) upper incisor dimensions in the flow direction,
- 7 (2) upper teeth position with respect to the palatal plane.

8 Based on the incisor inclinations reported in Fredericks [1974] and Ellis and McNama-
 9 rama [1986] the angles of the trapezoid with respect to the palatal plane denoted
 10 θ_1 and θ_2 are set as: $\theta_1 = 107^\circ$ and $\theta_2 = 90^\circ$. The upper parallel side or the
 11 base of the trapezoid coincides with the palatal plane l_{pal} and the lower parallel
 12 side represents the teeth tip l_t . The tip length in the main flow direction [Rudolph
 13 *et al.*, 1998] is set to $l_t = 1.25$ mm and the height h_t [Magne *et al.*, 2003] is set to
 14 17.5 mm which is within the range observed on 'in-vivo' data [Rudolph *et al.*, 1998;
 15 Magne *et al.*, 2003]. Consequently, the base of the trapezoid yields $l_{\text{pal}} = 6.6$ mm.
 16 The distance indicated as l_0 in Fig. 1(a) corresponds morphologically to the dis-
 17 tance between the trailing teeth edge and the trailing edge of the lips and is set
 18 to $l_0 \approx 1.7 \times l_{\text{pal}} = 11$ mm based on the ratios between teeth width and trailing
 19 lip position reported by McIntyre and Millett [2003]. The mentioned upper-teeth
 20 dimensions provide a two-dimensional palate-teeth shaped obstacle.

21 Next, a three-dimensional teeth-shaped nozzle is obtained by inserting the two-
 22 dimensional palate-teeth shaped obstacle in a rectangular channel representing a
 23 portion of the vocal tract, for which the upper wall represents the hard palate,
 resulting in a teeth-shaped nozzle. A longitudinal view of the resulting nozzle is

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1 schematically illustrated in Fig. 1(b). The width w of the channel is fixed to $w =$
 2 105 mm and the inlet height of the channel is set to $h_0 = 25$ mm, so that the
 3 aspect ratios, both in the unconstricted and constricted region, are superior to 1,
 4 $w/h_0 \approx 4$ and $w/h \approx 14$ with $h = h_0 - h_t$ the aperture height. Consequently, the
 5 flow is expected to be two-dimensional. The contraction ratio h_0/h yields ≈ 3.3
 6 resulting in a $\pm 70\%$ obstruction degree. The length of the channel downstream the
 7 constriction ranges from $x = 0$ up to $x/h = 1.5$.

3. Numerical Simulation of the Airflow Through the Nozzle

9 The airflow is simulated with Large Eddy Simulation (LES) for incompressible
 10 unsteady flows. The dynamic Smagorinsky model [Germano *et al.*, 1991] with mod-
 11 ification due to Lilly [1992] is used so that the Smagorinsky coefficient C_s is deter-
 12 mined locally in space and time. Simulations are obtained with a general-purpose
 13 finite element code *Front Flow Blue/FFB 5* on a supercomputer (SX8 NEC Inc.)
 14 [Kato and Ikegawa, 1991; Guo *et al.*, 2006].

15 The downstream section of the computational domain matches the teeth-shaped
 16 nozzle defined in Sec. 2. The simulation geometry upstream the teeth-shaped obsta-
 17 cle consists in a uniform rectangular section matching the channel height h_0 and
 18 width w of the teeth-shaped obstacle nozzle illustrated in Fig. 1(b). The total length
 19 upstream the teeth-shaped obstacle yields $3.2h_0$. Structured meshes are used to gen-
 20 erate the computational grid of 18,82,200 elements (Gridgen v1.5, Pointwise Inc.).
 21 The grid meshes are refined close to and downstream the obstacle in order to resolve
 22 the boundary layer. The quality of the mesh was extensively verified as well as the
 23 Courant–Friedrichs–Lewy number during simulation. A uniform velocity profile is
 24 imposed at the inlet of the computational domain. No-slip boundary conditions are
 25 used at the wall whereas non-reflective conditions are imposed at the outlet. The
 26 averaged grid accuracy at and downstream of the constriction yields 0.13 mm and
 27 increases to 0.05 mm along the boundaries.

28 The non-dimensional time increment Δt is set so that $10^{-3} = \Delta t \cdot U_b / h_0$ with U_b
 29 the bulk velocity at the inlet and h_0 the unconstricted nozzle height. The Reynolds
 30 number is set to $Re = 4000$ so that the bulk velocity yields $U_b = 2.5$ m/s. An
 31 overview of imposed geometrical and flow parameters is given in Table 1. Mean and
 32 fluctuating characteristics of the velocity field are quantified on 5000 instantaneous
 33 flow fields obtained from time step 5000 up to 10,000.

4. In-Vitro Experimental Setup and Nozzle

4.1. ‘In-vitro’ experimental conditions and nozzle

35 Airflow is generated in a flow facility consisting of an air compressor (Atlas Copco
 36 GA7) followed by a manual valve and pressure regulator (Norgren type 11-818-
 37 987) enabling one to provide constant air pressure. A uniform duct of diameter

Table 1. Overview of flow conditions and nozzle characteristics for LES simulations and 'in-vitro' experiments.

	LES	'in-vitro'
Nozzle width, w		105 mm
Nozzle length, l	97 mm	59.5 mm
Nozzle height, h_0		25.0 mm
Nozzle wall thickness, th	0 mm	6 mm
Trailing obstacle edge from outlet, l_0		11.0 mm
Tip length of the obstacle, l_t		1.25 mm
Leading obstacle angle, θ_1		107°
Trailing obstacle angle, θ_2		90°
Minimum aperture, h		7.5 mm
Inlet Reynolds number, Re		4000
Inlet bulk velocity, U_b		2.5 m/s
Volume airflow rate, ϕ		363 l/min

1 1cm connects the pressure regulator to a short convergent-divergent diffuser with
 2 total length 7 cm and outlet diameter 25 mm. The diffuser is attached to a settling
 3 chamber of volume 0.12 m³ with dimensions 600 × 510 × 415 mm (length × width ×
 4 height). Grids are used in the settling chamber to reduce turbulence intensity so
 5 that the streamwise turbulence intensity at the nozzle inlet is below 1%.

6 The rectangular rigid nozzle, described in Sec. 2, was mounted at the exit of the
 7 settling chamber. The constriction geometry is shaped in accordance with Sec. 2, so
 8 that the nozzle represents a simplified 'in-vitro' replica of a teeth-shaped obstacle
 9 in the upper airways. The resulting nozzle geometry and setup are schematically
 10 illustrated in Fig. 2. The main 'in-vitro' nozzle characteristics are summarised in
 11 Table 1. The nozzle geometry was obtained as a three-dimensional plaster print from
 the numerical grid (3D Digital Service OURA Inc.). Consequently, the 'in-vitro'

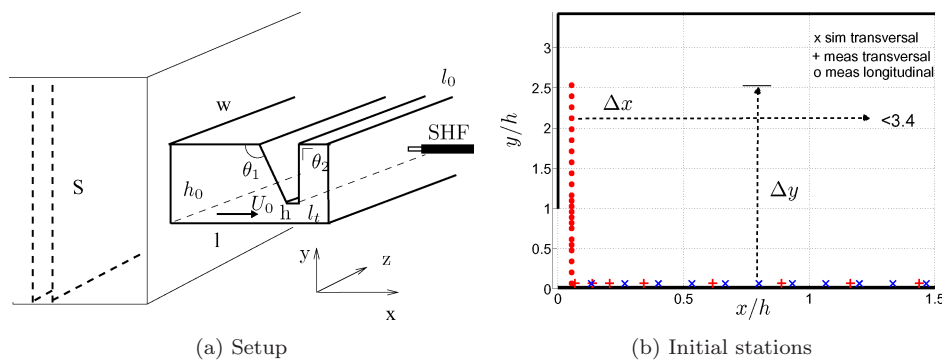


Fig. 2. (a) Schematic illustration of experimental setup and 'in-vitro' teeth-shaped nozzle. Symbols are as defined in Table 1 and Fig. 1 with SHF denoting stationary hot film (SHF) anemometry. The main flow direction is indicated by a bold arrow. (b) Initial data stations for transverse ($y < 0.5$ mm and $\Delta y = 0.1$ mm) and longitudinal ($x < 0.5$ mm $\Delta x = 0.1$ mm) profiles gathered downstream the trailing edge of the teeth, corresponding to $x/h = 0$ and $y/h = 1$, for SHF measurements (transverse +, longitudinal o) are indicated. In addition, transverse profiles taken from simulations (x) for comparison are given as well.

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1 geometry matches the computational grid applied in the numerical simulations
2 except for the channel length upstream the obstacle as seen from Table 1. The
3 upstream channel length in the computational grid yields 80 mm compared to 42 mm
4 in the ‘in-vitro’ replica.

5 **4.2. Single sensor anemometry**

6 Velocity measurements were made by constant temperature anemometry (IFA300)
7 at a Reynolds number $Re = 4000$ based on the inlet height h_0 and the inlet bulk
8 velocity $U_b = 2.5$ m/s corresponding to a volume airflow rate $\phi = 363$ l/min. A single
9 sensor hot film (TSI 1201-20) with a diameter of $50.8 \mu\text{m}$ and a working length of
10 1.02 mm was traversed in the x , y and z directions by means of a two-dimensional
11 stage positioning system (Chuo precision industrial co. CAT-C, ALS-250-C2P and
12 ALS-115-E1P). The accuracy of positioning in the longitudinal x and perpendicular
13 y or z direction yields 4 and $2 \mu\text{m}$, respectively.

14 The single sensor hot film was positioned perpendicular to the x direction cor-
15 responding to a film yaw angle $\alpha = 0^\circ$. The film position is parallel to the z axis
16 to enhance spatial accuracy in the y direction, except when the two-dimensionality
17 of the flow is verified along the z axis for which the film is parallel with the y axis.
18 The stem was varied to a pitch angle $\beta = 11^\circ$ in order to measure the flow veloc-
19 ity near the wall and to limit flow disturbances induced by the probe stem. The
20 hot-film is calibrated against mean velocities given by a thermal mass flow meter
21 (TSI 4040). A fourth-order polynomial law is fitted to the anemometers output
22 voltage in order to convert the measured voltage to velocity. The measured output
23 voltages are corrected for temperature variations, boundary layer development and
24 wall proximity on a ninth-order convergent nozzle ensuring a top-hat outlet profile
25 and turbulence intensities below 1% [Bruun, 1995; Johnstone *et al.*, 2005]. Applied
26 voltage corrections are well below the obtained accuracy of 0.1 m/s in the velocity
27 range of interest. At each measurement station velocity data are gathered during
28 4 s consecutively at a sampling frequency of 40 kHz.

29 **4.3. Measurement Stations**

30 The near flow field of the jet issuing from the constriction h is experimentally
31 scanned in the longitudinal x -direction and in the traverse y -direction. The initial
32 measurement stations are situated at less as 0.5 mm from the wall coinciding with
33 either the flat bottom plate for the transverse or the trailing teeth edge for the lon-
34 gitudinal profiles as schematically indicated in Fig. 2(b). The displacement Δx and
35 Δy is set to 0.1 mm in order to ensure high spatial accuracy, e.g. 68 measurement
36 stations from the initial station up to $y/h = 1$ in the transverse profile. Transverse
37 data parallel with the y -axis are gathered up to $y/h = 2.5$ or 185 measurements
38 for each initial x -station. All transverse measurement stations are situated between
39 $0 < x < 11$ mm downstream the constriction up to the nozzle exit. The longitu-
dinal direction is scanned from the initial stations up to $x/h = 3.4$, which results

1 in 249 measurement stations for each initial y -station. Consequently, longitudinal
 2 measurements are gathered downstream the constriction up to 14 mm in free space
 3 downstream the nozzle exit.

5. Results and Discussion

5 The computed and measured velocity flow field is systematically compared for the
 6 measurement stations indicated in Fig. 2(b). This way a detailed comparison of
 7 the flow development in the near field from $0 < x/h < 1.5$, i.e. downstream the
 8 constriction at $x = 0$ up to the nozzle exit, is obtained. A quantitative comparison
 9 of the mean and fluctuation part of the velocity is performed in the next subsections.

10 Since the anemometry data inform on the magnitude of the velocity, denoted U ,
 11 and not on a single component, the magnitude of the simulated velocity is considered
 for the comparison, except when explicitly mentioned.

13 5.1. Constriction outlet conditions: initial transverse profile

14 The mean and rms of the measured ($x/h = 0.06$) and simulated ($x/h = 0.13$) initial
 15 transverse velocity profiles downstream the obstruction, are presented in Fig. 3.
 16 Some similarities and dissimilarities between measured and simulated profiles are
 17 observed.

18 The presence of the obstruction on one side and a flat wall on the other side is
 19 expected to provoke an asymmetry in the mean velocity profile. This asymmetry is
 indeed observed in the simulated as well as the measured mean profiles. However, the
 21 measured and simulated flow profiles indicate a different flow development due to

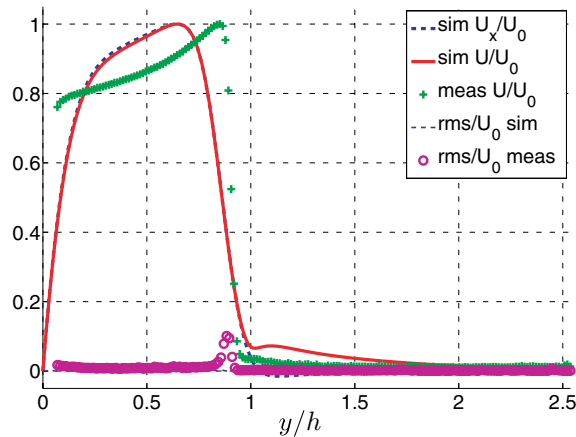


Fig. 3. Mean and fluctuating (rms) portions of the initial measured ($x/h = 0.06$, meas) and simulated ($x/h = 0.13$, sim) transverse velocity profile downstream the obstruction: U denotes the magnitude of the velocity normalised with the maximum velocity in the initial transverse profile U_0 and U_x the component along the x -axis.

1 the presence of different velocity gradients. It is clearly seen that the mean velocity
 2 profile at the outlet can be described roughly by three consecutive growth rates
 3 dU/dy , whereas more are needed to describe the measured profiles. In addition, the
 4 position of the maximum velocity U_0 is shifted towards $y/h = 1$ and the overall
 5 jet width is significantly larger for the measured data compared to the simulated
 6 data. For completeness besides the magnitude also the x -component of the simu-
 7 lated velocity U_x field is plotted. It is seen that for $y/h < 1$ the difference between
 8 the magnitude and the U -component is small ($< 1\%$). Although for $y/h \geq 1$ an
 9 important discrepancy between both quantities is observed due to the presence of
 10 a recirculation zone in which the contribution of the x -component of the velocity
 11 is small compared with the y -component. Since the anemometry data are obtained
 12 with a single film mounted parallel to the y -axis, the film is less sensitive to the
 13 y -component and consequently the measurement less accurate. Therefore, the mea-
 14 sured velocity for $y/h \geq 1$ is comprised between the magnitude of the simulated
 15 x -component and the magnitude of the velocity simulation.

16 The overall turbulence level at the outlet is $< 2\%$ for the measured as well as the
 17 simulated data. Nevertheless, the asymmetry in the measured mean velocity data is
 18 associated with a local turbulence peak exceeding 10%. The absence of such a peak
 19 in the simulated data is associated with the different position y_m/h of maximum
 20 mean velocity U_0 with respect to the aperture edge at $y/h = 1$.

21 Therefore, despite the matching geometry and flow conditions for the simulated
 22 and measured data, some important differences in the initial outlet profiles down-
 23 stream the constriction are observed.

5.2. *Transverse mean velocity profiles*

24 The characterisation of the development of the mean measured and simulated veloc-
 25 ity profiles in the near field downstream the constriction is based on the quantities
 26 schematically indicated in Fig. 1(b), i.e. $y_m(x)$ distance from the wall up to max-
 27 imum flow velocity $U_m(x)$ and $y_{1/2}(x)$ distance from the wall up to $U_m(x)/2$. In
 28 addition, the jet width Δy_w is sought. The characteristic velocity at the con-
 29 striction outlet U_0 is defined as the maximum velocity of the initial transverse mean
 30 velocity profile discussed in the previous subsection.

31 The transverse profiles are obtained for downstream positions ranging from the
 32 obstruction up to the nozzle exit, i.e. $0 < x/h < 1.5$ as shown in Fig. 2. An overview
 33 of the measured and simulated mean velocity profiles is shown in Fig. 4. The growth
 34 rate of the jet and the asymmetry of the profiles are sought by considering the down-
 35 stream evolution of the position $y_m(x/h)$ corresponding to the maximum velocity
 36 $U_m(x/h)$ for each profile, the outer position $y_{1/2}(x/h)$ corresponding to half the
 37 maximum velocity $U_m/2(x/h)$ and the ratio of the maximum velocity within each
 38 profile $U_m(x/h)$ to the characteristic velocity U_0 . The resulting quantities $y_m(x/h)$,
 39 $y_{1/2}(x/h)$ and $U_m(x/h)/U_0$ are illustrated in Figs. 5(a) and 5(b). The position
 40 of maximum velocity $y_m(x)/h$ is seen to decrease for the measured as well as the
 41

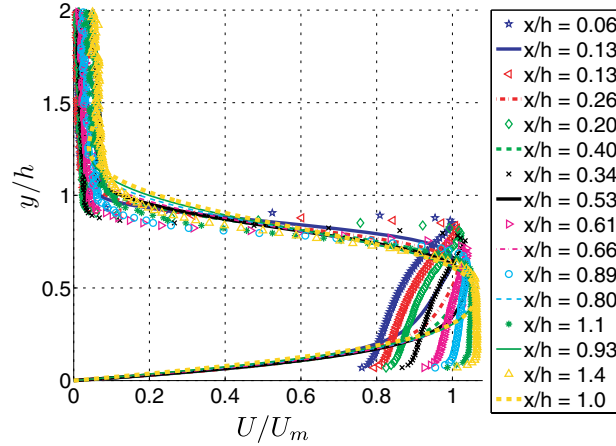


Fig. 4. Measured (symbols) and simulated (lines) transverse mean velocity profiles for $0 < x/h < 1.5$. The magnitude of the profiles normalised with the characteristic velocity U_0 is plotted. U_0 corresponds to the maximum of the initial transverse profile discussed in Sec. 5.1.

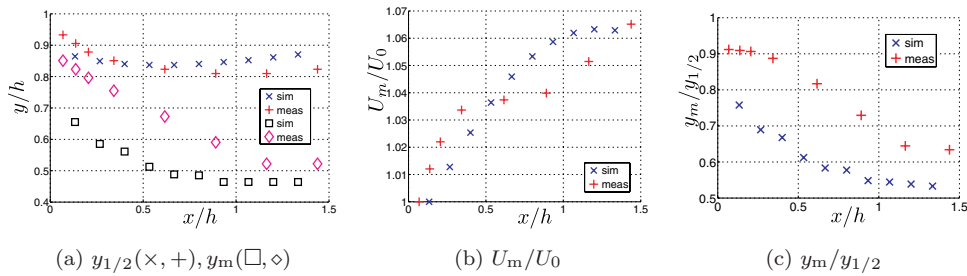


Fig. 5. Measured (meas) and simulated (sim) downstream evolution, $0 < x/h < 1.5$, for (a) the position of maximum velocity and the outer position of half the maximum velocity $y_{1/2}$ (simulated = \times and measured = $+$) and y_m (simulated = \square and measured = \diamond), (b) the ratio of the maximum velocity to the characteristic outlet velocity U_m/U_0 and (c) the ratio of the positions y_m and $y_{1/2}$, i.e. $y_m/y_{1/2}$.

1 simulated profiles. Nevertheless, measured $y_m(x)/h$ -values continue to decrease until
 3 $x/h \geq 1.1$ is reached, whereas a nearly constant value ($\pm 2\%$) is attained for simu-
 lations $y_m(x/h \geq 0.7)/h \approx 0.47$. So $y_m/h \approx \text{constant}$ is postponed on the measured
 data compared to the simulated data.

5 The outer position $y_{1/2}$, corresponding to half the maximum velocity U_m , shows
 a decrease followed by an increase for both the measured as well as simulated
 7 velocity data for increasing x/h -values. Although, the observed increase of $y_{1/2}$
 on the measured data, $x/h \geq 1.1$, is postponed with respect to the simulated data,
 9 $x/h \geq 0.7$. Moreover, a constant y_m range and increase of $y_{1/2}$ are seen to occur at
 approximately the same downstream positions x/h , i.e. $x/h \geq 1.1$ and $x/h \geq 0.7$
 11 for the measured and simulated data, respectively.

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1 Figure 5(c) illustrates the resulting ratio $y_m/y_{1/2}$. As before, measured and sim-
 3 ulated data exhibit the same overall tendency, i.e. a decrease until a constant value
 5 is reached. In addition, again the downstream x/h station for which a constant
 7 regime is approximated is postponed when comparing measured to simulated data.
 9 The ratio $y_m/y_{1/2}$ is a simple measure on the (a)-symmetry of the jet develop-
 11 ment. In general the initial decrease of the measured and simulated ratios indicates
 13 an increased symmetry of the jet. Note that $y_m/y_{1/2} \approx 0.9$ as observed for the
 15 measured profiles immediately downstream the obstacle indicates that y_m and $y_{1/2}$
 17 almost coincides, which indicates a large velocity gradient in the outer layer near
 19 the teeth edge. Such a large gradient will favor vorticity stretching for $y/h \approx 1$,
 21 whereas a shifted position of maximum velocity towards $y/h \approx 1$ will favor vorticity
 23 convection for transverse positions with $y/h \approx 1$.

25 The ratio $y_m/y_{1/2}$ provides a first quantification of the asymmetry of the jet
 27 development. In addition, the evolution of a jet width Δy_w corresponding to a
 mean velocity larger as a certain percentage p of $U_m(x)$, i.e. $U(y/h, x/h) > p \times$
 $U_m(x/h)/100$, is sought. Figure 6 illustrates the jet width Δy_w for percentages
 derived on the measured transverse velocity profiles. Firstly, for each downstream
 position $0 < x/h < 1.5$, a variable percentage p is determined for each transverse
 profile on the first transverse velocity measurement near the wall, i.e. $y/h \leq$
 0.07 as $p(x/h) = U(y/h \leq 0.07, x/h)/U_m(y_m, x/h) \times 100$. Resulting percentages
 $p(x/h)$ are depicted in Fig. 6(b). The retrieved percentages $p(x/h)$ increase gradually
 up to 97% from the trailing edge of the obstacle up to the nozzle exit and yield,
 respectively, 77, 79, 81, 84, 90, 92, 94, 96, 97 and 97%. Secondly, p is fixed to
 97%, i.e. the maximum percentage determined by the measured near-wall velocities.
 Consequently, $\Delta y_w(x/h, p = 97\%)$ involves all transverse measurement stations
 for which the velocity exceeds $0.97 \times U_m(x/h)$. The fixed percentage $p = 97\%$ is
 indicated in Fig. 6(b) as well.

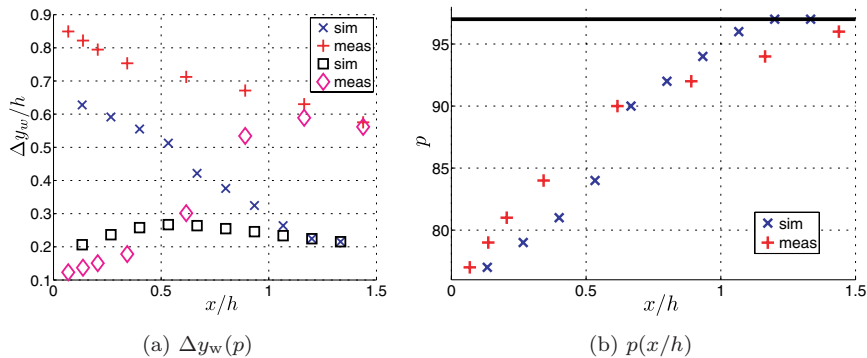


Fig. 6. The jet width Δy_w for different downstream stations $0 < x/h < 1.5$ is shown in Fig. 6(a) (1) for p fixed to 97% (simulated \square , measured \diamond) and (2) for variable percentage $p(x/h)$ (simulated \times , measured $+$) determined on the measured near wall value at $y/h \leq 0.07$ as $U(y/h \leq 0.07, x/h)/U_m(y_m, x/h) \times 100$. The resulting percentages $p(x/h)$ are illustrated in Fig. 6(b) where the fixed percentage $p = 97\%$ is indicated by a solid line.

1 For $x/h \geq 1$ the variable percentages are close to the fixed percentage $p = 97\%$
 2 so that the resulting jet widths Δy_w are approximately the same as can be seen in
 3 Fig. 6(a). Consequently, for $x/h \geq 1$ the jet width Δy_w observed for $p = 97\%$ on
 4 the measured profiles is almost three times the jet width obtained from simulated
 5 data. Despite a slight increase-decrease tendency for x/h smaller are greater than
 6 0.6, the jet width Δy_w ($p = 97$) observed for the simulated data is fairly constant,
 7 i.e. $0.2 < \Delta y_w < 0.28$. For the measured transverse profiles, the jet width is seen to
 8 broaden for increasing x/h so that $0.1 < \Delta y_w < 0.6$. A steep increase occurs from
 9 $\Delta y_w \approx 0.3$ to $\Delta y_w \approx 0.55$ as $x/h > 0.7$. The initial occurrence of small jet widths
 10 $\Delta y_w < 0.2$ is due to the large asymmetry involving a narrow peak superposed on
 11 the measured transverse velocity profile for small x/h as is easily observed on the
 12 initial profile at $x/h = 0.06$ shown in Fig. 3. This peak is absent in the simulated
 13 profiles, so that small $\Delta y_w < 0.2$ are not observed for the simulated transverse
 14 profiles. The broadening of Δy_w for $x/h > 0.7$ is associated with the disappearance
 15 of such a peak.

16 The percentage p -value set to $p = 97\%$ allows to detect such narrow peaks, but
 17 are not suitable to consider the overall jet width. Therefore, the jet width Δy_w
 18 is re-evaluated with p -values set as $p(x/h) = U(y/h \leq 0.07, x/h)/U_m(y_m, x/h) \times$
 19 100 . The resulting jet width Δy_w is decreasing with x/h for simulated as well as
 20 measured profiles. Despite the general tendency, the decrease more pronounced for
 21 the simulated than for the measured data. In addition, Δy_w is seen to be 1.3 up to
 22 2.6 times larger for the measured than for the simulated profiles.

23 5.3. Transverse rms profiles

24 Figure 7 shows the rms values of the measured and simulated velocity profiles for
 25 which the mean values are shown in Fig. 4. Simulated rms values are below 2%
 26 regardless the spatial position of the measurement station. The measured profiles
 27 on the other hand exhibit a peak in the turbulence intensity up to 10% near the
 28 obstacle edge. The evolution of the spatial position of the maximum rms value
 29 for $0 < x/h < 1.5$ is depicted in Fig. 8(a). As a reference, the position of the
 30 maximum mean velocity is indicated for each x/h station as well. The maximum
 31 turbulence intensity for the measured profiles shifts from $y/h \approx 0.9$ at $x/h = 0.06$
 32 down to $y/h \approx 0.8$ at $x/h > 0.5$. The maximum mean velocity y_m is seen to pre-
 33 ceede the maximum turbulence intensity, which occurs closer towards the obsta-
 34 cle edge and therefore for larger y/h values. The discrepancy between y_m and
 35 maximum turbulence position is increasing for $x/h > 0.7$ since y_m is decreasing
 36 while the maximum turbulence position is maintained. For the simulated profiles
 37 on the other hand no peak is observed since the turbulence intensity is below 1%.
 38 The maximum values occur for $y/h \approx 0.5$. Although due to the low turbulence
 39 intensities, the simulated flow is laminar in contrast to the measured flow for which
 40 turbulence is seen to be generated near the edge of the obstacle and is convected
 41 downstream.

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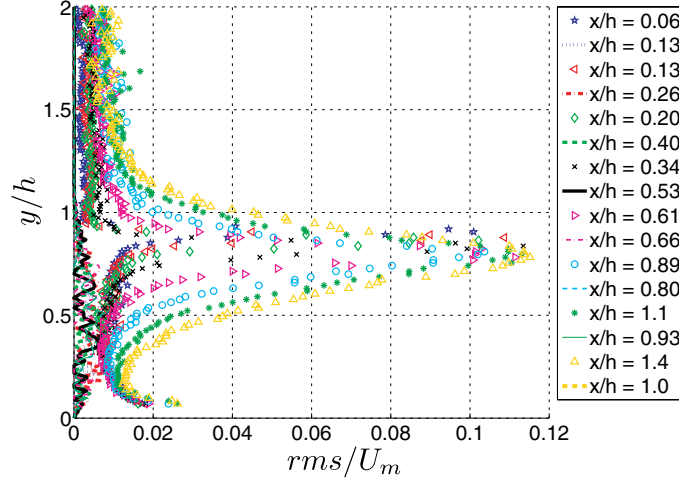


Fig. 7. Turbulence intensities associated to the measured (symbols) and simulated (lines) transverse velocity profiles shown in Fig. 4 for $0 < x/h < 1.5$.

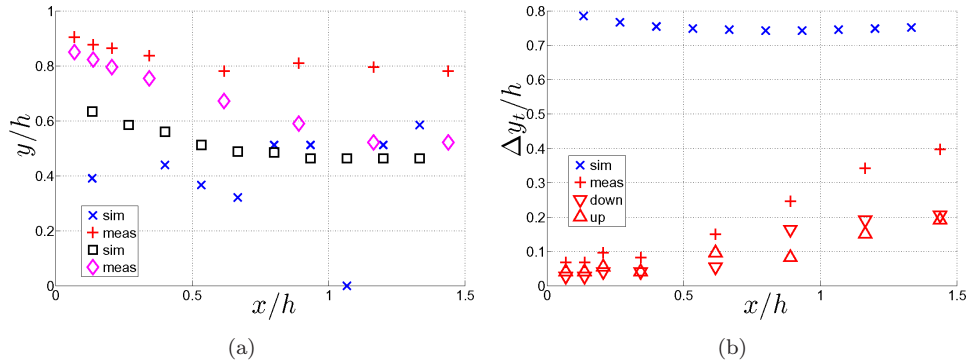


Fig. 8. (a) Position of maximum turbulence intensity in the measured (+) and simulated (x) profiles shown in Fig. 7 for $0 < x/h < 1.5$. The maximum mean velocity y_m is given for measured (\square) and simulated (\diamond) profiles. (b) The width of the turbulence peak for half the maximum value, $\Delta y_t/h$, for simulated (x) and measured (+) profiles. For measured profiles the half widths for y/h larger (\triangle) and smaller (∇) than the peak position are indicated as well.

1 The width of the turbulence peak Δy_t is considered in Fig. 8(b). A narrow tur-
 2 bulance peak, $\Delta y_t/h < 0.1$, is observed for small $0 < x/h < 0.34$. The peak is seen
 3 to broaden gradually up to $\Delta y_t/h \approx 0.4$ for $x/h = 1.5$. In addition, the symmetry
 4 of the turbulence peak is verified by considering the contribution to Δy_t for y/h -
 5 values, respectively, larger and smaller than the position of maximum turbulence
 6 intensity. Resulting values are indicated in Fig. 8(b). The small turbulence intensi-
 7 ties and absence of a peak observed for simulated data result in $\Delta y_t/h \approx 0.75$
 regardless x/h .

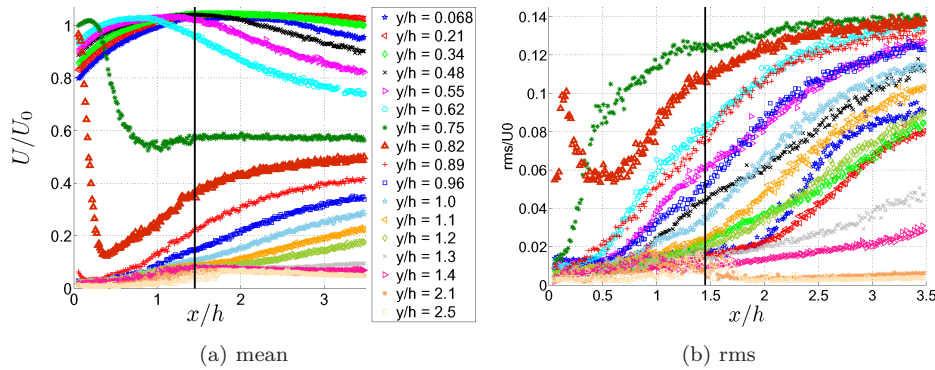


Fig. 9. Measured longitudinal (a) mean and (b) rms velocity profiles for the measurement stations indicated in Fig. 2(b). The nozzle exit at $x/h = 1.5$ is depicted by a solid line. Measured values for $y/h \approx 0.82$ (Δ) are indicated in bold.

1 5.4. Measured mean and rms longitudinal velocity profiles

2 In addition to the transverse velocity profiles, longitudinal velocity profiles are mea-
 3 sured for stations with $0 < y/h < 2.5$ and $0 < x/h < 3.5$ as indicated in Fig. 9. The
 4 estimated longitudinal mean and rms velocity profiles are given in Fig. 9. In general,
 5 the longitudinal profiles confirm the findings for the transverse velocity profiles for
 6 $x/h < 1.5$, e.g. the maximum in the mean velocity is seen to shift towards the wall
 7 and the jet width is seen to decrease when moving to more downstream observation
 8 positions. Although, no quantification is assessed since Δy between two longitudinal
 9 profiles is too broad to result in an accurate quantification. Nevertheless, a narrow
 10 turbulence peak and steep decrease of mean velocity is observed at $y/h \approx 0.82$ for
 11 $x/h < 0.2$.

6. Conclusion

13 The presented research provides experimental as well as numerical flow data in
 14 the near field of a two-dimensional jet issuing from a constriction for a flow with
 15 Reynolds number 4000. The constriction is obtained from a teeth-shaped obstacle
 16 placed in a rectangular channel so that the current geometrical and flow conditions
 17 are relevant to flow through the oral cavity. At term, the current study might con-
 18 tribute to very common applications dealing with a.o. human sound production. It is
 19 evident that the considered geometry, although derived from morphological incisor
 20 data, does not account for variation of important morphological features such as
 21 location, orientation, shape, constriction degree, tissue properties, etc. Nevertheless,
 22 to the knowledge of the authors, the current study is the first to account for such
 23 a geometry, involving both numerical and experimental flow data enabling one to
 24 validate numerical simulations. The near field is studied since a good characterisa-
 25 tion is needed in order to describe sound production due to the interaction of an
 airflow with the obstacle.

1 A first comparison between simulated and experimental velocity features is
2 obtained by quantifying features typically dealt with in studies of a plane wall
3 jet. This is motivated since the current problem is basically thought of as a two-
4 layer shear flow consisting of an inner layer (similar to a boundary layer) and an
5 outer layer (similar to a free shear layer) as is the case for a plane wall jet. Neverthe-
6 less, the current results, numerical as well as experimental, show that the interaction
7 between the two generic layers leads to a more complex near flow field for which more
8 layers can be distinguished. Therefore, future studies should consider the flow field
9 in more detail; i.e. involving both the near and the fully developed region in order
10 to validate established self-similar models and scaling laws for the plane wall jet.

11 From the comparison of the experimental and simulated flow features, it is seen
12 that the mean flow fields show the same general tendencies, but differ when consid-
13 ering the quantified features. The main common observations for the mean velocity
14 include: (1) the position of maximum velocity y_m shifts towards the wall for increas-
15 ing downstream position, (2) the maximum mean velocity U_m increases downstream
16 the constriction, (3) the jet width is seen to decrease for increasing downstream
17 position, (4) as does the ratio of the position of maximum velocity to the outer
18 half width $y_m/y_{1/2}$. Nevertheless, some important differences are observed from
19 the quantified mean velocity features with respect to the structure of the jet: (1)
20 the experimentally observed jet is broadened compared to the numerical jet, (2) the
21 experimental mean velocity exhibits a narrow peak for $y/h \approx 1$, which is absent for
22 the simulated data, (3) the position of maximum velocity is reached for $y/h \approx 1$
23 on the experimental data, which is larger than for the simulated data and finally
24 (4) the ratio of the position of maximum velocity to the outer half width $y_m/y_{1/2}$
25 is close to one for the experimental data. The observed differences are the result
26 of increased mean velocity and mean velocity gradients in the vicinity of the teeth
27 edge, i.e. $y/h \approx 1$, for the experimental data compared to the simulated data. Both
28 observations are important considering vorticity. The narrow peak near the teeth
29 edge, observed on the measured mean velocity profiles, is accompanied with a nar-
30 row symmetrical peak in turbulence intensity up to 10%. The observed peak is
31 absent in the simulated flow field, which is laminar in the near field downstream the
32 constriction. Consequently, the observed differences in mean and turbulence inten-
33 sities encourage further research in particular when sound production is of interest.
34 It should be noted that although more accurate measurements can be performed,
35 e.g. by using other measurement techniques, the observed differences largely exceed
36 the uncertainty of the velocity measurements and are therefore significant.

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